### **AFRL-ML-WP-TP-2007-421**

## PURIFICATION OF CONTAMINATED MIL-PRF-83282 HYDRAULIC FLUID USING THE PALL PURIFIER AND MULTIPLE PROCESS CONFIGURATIONS (PREPRINT)



Carl E. Snyder, Jr., Lois J. Gschwender, Stephen L. Gunderson, and George W. Fultz

#### **NOVEMBER 2006**

Approved for public release; distribution unlimited.

#### **STINFO COPY**

The U.S. Government is joint author of this work and has the right to use, modify, reproduce, release, perform, display, or disclose the work.

MATERIALS AND MANUFACTURING DIRECTORATE AIR FORCE RESEARCH LABORATORY AIR FORCE MATERIEL COMMAND WRIGHT-PATTERSON AIR FORCE BASE, OH 45433-7750

#### NOTICE AND SIGNATURE PAGE

Using Government drawings, specifications, or other data included in this document for any purpose other than Government procurement does not in any way obligate the U.S. Government. The fact that the Government formulated or supplied the drawings, specifications, or other data does not license the holder or any other person or corporation; or convey any rights or permission to manufacture, use, or sell any patented invention that may relate to them.

This report was cleared for public release by the Air Force Research Laboratory Wright Site (AFRL/WS) Public Affairs Office and is available to the general public, including foreign nationals. Copies may be obtained from the Defense Technical Information Center (DTIC) (http://www.dtic.mil).

AFRL-ML-WP-TP-2007-421 HAS BEEN REVIEWED AND IS APPROVED FOR PUBLICATION IN ACCORDANCE WITH ASSIGNED DISTRIBUTION STATEMENT.

\*//Signature//

CARL E. SNYDER, JR., Program Manager Nonstructural Materials Branch Nonmetallic Materials Division //Signature//

STEPHEN L. SZARUGA, Acting Chief Nonstructural Materials Branch Nonmetallic Materials Division

//Signature//

SHASHI K. SHARMA, Acting Deputy Chief Nonmetallic Materials Division Materials and Manufacturing Directorate

This report is published in the interest of scientific and technical information exchange, and its publication does not constitute the Government's approval or disapproval of its ideas or findings.

<sup>\*</sup>Disseminated copies will show "//Signature//" stamped or typed above the signature blocks.

#### REPORT DOCUMENTATION PAGE

Form Approved OMB No. 0704-0188

The public reporting burden for this collection of information is estimated to average 1 hour per response, including the time for reviewing instructions, searching existing data sources, searching existing data sources, gathering and maintaining the data needed, and completing and reviewing the collection of information. Send comments regarding this burden estimate or any other aspect of this collection of information, including suggestions for reducing this burden, to Department of Defense, Washington Headquarters Services, Directorate for Information Operations and Reports (0704-0188), 1215 Jefferson Davis Highway, Suite 1204, Arlington, VA 22202-4302. Respondents should be aware that notwithstanding any other provision of law, no person shall be subject to any penalty for failing to comply with a collection of information if it does not display a currently valid OMB control number. PLEASE DO NOT RETURN YOUR FORM TO THE ABOVE ADDRESS.

1. REPORT DATE (DD-MM-YY)	2. REPORT TYPE		3. DATES CO	OVERED (From - To)
November 2006	Paper Preprint	t		
4. TITLE AND SUBTITLE				5a. CONTRACT NUMBER
PURIFICATION OF CONTAMIN	ATED MIL-PRF-8	3282 HYDRAULIC F	LUID	FA8650-05-D-5050
USING THE PALL PURIFIER AN	ID MULTIPLE PR	OCESS CONFIGURA	TIONS	5b. GRANT NUMBER
(PREPRINT)				5c. PROGRAM ELEMENT NUMBER 62102F
6. AUTHOR(S)				5d. PROJECT NUMBER
Carl E. Snyder, Jr. and Lois J. Gsch	wender (AFRL/M	LBT)		4347
Stephen L. Gunderson and George	W. Fultz (Universi	ty of Dayton Research	Institute)	5e. TASK NUMBER
				60
				5f. WORK UNIT NUMBER
				61100002
7. PERFORMING ORGANIZATION NAME(S) A Nonstructural Materials Branch (AFRL/MI Nonmetallic Materials Division Materials and Manufacturing Directorate Air Force Research Laboratory, Air Force I Wright-Patterson Air Force Base, OH 4543	LBT)  Materiel Command	University of Dayton R Institute 300 College Park Dayton, OH 45469	esearch	8. PERFORMING ORGANIZATION REPORT NUMBER
9. SPONSORING/MONITORING AGENCY NAM	• •	ES)		10. SPONSORING/MONITORING AGENCY ACRONYM(S)
Materials and Manufacturing Direc	torate			AFRL-ML-WP
Air Force Research Laboratory				
Air Force Materiel Command Wright-Patterson AFB, OH 45433-	7750			11. SPONSORING/MONITORING AGENCY REPORT NUMBER(S) AFRL-ML-WP-TP-2007-421
12. DISTRIBUTION/AVAILABILITY STATEMENT Approved for public release; distribution	= =			
13. SUPPLEMENTARY NOTES  The U.S. Government is joint authorous disclose the work. PAO Case No.				
14. ABSTRACT The amount of hydraulic fluid used	by all branches of	the military is significa	ant both in t	erms of volume and cost. The

The amount of hydraulic fluid used by all branches of the military is significant both in terms of volume and cost. The disposal of used hydraulic fluid is a cost, time, and logistical component that can be greatly reduced by the purification and reuse of used hydraulic fluid. This report describes a project that evaluated the effectiveness of various hydraulic fluid purification process configurations on the removal of water and particulate contaminants from MIL-PRF-83282 hydraulic fluid in 55-gallon drums.

#### 15. SUBJECT TERMS

Hydraulic fluid, purification, contaminants, MIL-PRF-83282

16. SECURITY CLASSIFICATION	l OF:	17. LIMITATION	18. NUMBER	19a. NAME OF RESPONSIBLE PERSON (Monitor)
a. REPORT Unclassified  b. ABSTRACT Unclassified Unclassified	c. THIS PAGE Unclassified	OF ABSTRACT: SAR	OF PAGES 22	Care E. Snyder, Jr.  19b. TELEPHONE NUMBER (Include Area Code) N/A

Standard Form 298 (Rev. 8-98) Prescribed by ANSI Std. Z39-18

# Purification of Contaminated MIL-PRF-83282 Hydraulic Fluid using the Pall Purifier and Multiple Process Configurations

#### **Introduction**

The amount of hydraulic fluid used by all branches of the military is significant both in terms of volume and cost. The disposal of used hydraulic fluid is a cost, time, and logistical component that can be greatly reduced by the purification and reuse of used hydraulic fluid. This report describes a project that evaluated the effectiveness of various hydraulic fluid purification process configurations on the removal of water and particulate contaminants from MIL-PRF-83282 hydraulic fluid in 55-gallon drums.

#### **Materials and Methods**

The fluid used in this evaluation was fresh MIL-PRF-83282 hydraulic fluid that was contained in a 55-gallon drum. The actual fluid amount contained in the drum and subjected to the purification process was approximately 53 gallons. The purifier used in the tests was a Pall portable purification unit model #PE-00440-1Z (Figure 1) and all testing was carried out under ambient conditions (above 60°F/15°C). A slurry of natural Arizona road dust containing particles of various sizes was introduced into clean MIL-PRF-83282 and used to simulate particulate contamination. Laboratory-supplied distilled water was used for the water contaminant.

Sampling of the fluid was accomplished by inserting one end of a ½" outside diameter glass tube into the drum and the other end fixed to a clean collection flask then drawing up approximately 6 oz. of the fluid into the flask by applying a slight vacuum (Figure 2). The fluid in the flask was then transferred to a clean sample bottle for analyses. The glass tubing and collection flasks were thoroughly washed with filtered hexane between sampling sets then the tube purged with N<sub>2</sub> and the flasks heated in an air-circulating oven at 200°C for 1 hour. During a second run using the two-drum purification process configuration, a new sampling technique was introduced that allowed the fluid to be drawn directly into the sample bottle so there would be no need to use a collection flask (Figure 3). This eliminated the fluid transfer step from the flask to the bottle and also the need to wash the sampling flasks after each sample was taken. The new technique utilized a vacuum connector between the end of the sampling tube and the sample bottle. Applying a slight vacuum to the connector allowed the fluid to be drawn up the tube, through the connector and into the sample bottle. However, due to the increased length on the receiving end of the glass sampling tube caused by the vacuum connector, the inlet/suction end of the glass tube was not long enough to reach the bottom fluid sample so the original vacuum flask sampling technique was used for the bottom fluid section sample. The glass tube was still washed as previous with the vacuum connector being washed in the same manner as the tube.

Samples were analyzed using a HIAC Royco model 8000A automatic particle counter and Karl-Fisher model 447 Coulomatic Titrimeter to determine the amount of particle and water contamination, respectively. Gravimetric analysis was performed in place of or in addition to using the automatic particle counter for several of the sample sets.

#### **Procedure**

This project evaluated two different purification process configurations. The first configuration utilized a "two-drum" set-up where the contaminated fluid was passed from its original drum, through the purifier then into a clean empty drum (Figure 4). This was followed by cycling the fluid between the purifier and the second or "clean" drum only (Figure 5). The second configuration utilized a "single-drum" setup where the contaminated fluid was cycled only between the purifier and the original fluid drum. Various lengths of discharge tubing (12, 18 and 24 inches) were evaluated within the single-drum purification method to determine if this had any effect on the results of the purification process.

Before starting the very first test, the new, clean fluid was sampled from the top (~2" below fluid surface), middle and bottom (~2" from drum bottom) and analyzed for particulate and water content as a baseline and to determine how much of each contaminant had to be added prior to starting the experiment. Water content was <100 ppm, the particulate level was NAS 1638 Class 6 and the gravimetric analysis was <1.0 mg/mL. While the specification limit for particulates in new MIL-PRF-83282 hydraulic fluid is NAS 1638 Class 5, this is not expected for fluid stored in drums because drums are allowed to "breathe". Then, while stirring the clean hydraulic fluid using an air-driven mixer, the particulate slurry was added until a sample drawn from the middle of the fluid registered a particle reading of NAS 1638 Class 12 or a gravimetric reading >1.0 mg/mL. Then, distilled water was added until the middle sample registered 600-700 ppm of water. During the test run, samples were taken from the top, middle and bottom of the fluid at predetermined time intervals until the minimum cleanliness limits for MIL-PRF-83282 was reached (NAS 1638 Class 5 for particulates and/or <1.0 mg/mL and <100 ppm water).

#### **Two-Drum Purification Process Configuration**

Following the contamination of the clean hydraulic fluid used in the two-drum configuration, the mixer was stopped and removed and the fluid was allowed to settle for 72 hours prior to starting the purification process. Samples were taken at 24 hour intervals from the top, middle and bottom of the fluid in an attempt to document the kinetics of the settling process.

After the 72-hour settling time, a 32"-long 6061 T-6 steel inlet/suction tube was connected to a quick-disconnect assembly in the large bung-hole of the contaminated fluid drum lid. The bottom of the tube was situated approximately 2" from the bottom of the drum. The lid was then secured onto the drum. Next, the inlet/suction hose of the Pall purifier was attached to the other end of the quick-disconnect assembly of the contaminated fluid drum. The outlet/discharge hose from the Pall purifier was attached to a quick-disconnect assembly in the small bung-hole of a clean empty drum lid. A 12"-long 6061 T-6 steel tube having an inside diameter of approximately 3/4" was attached to the opposite end of the quick-disconnect assembly to discharge the fluid into the clean empty drum.

Prior to starting the purification process, venting of each of the drums to prevent vacuum and pressure buildup was accomplished by loosening the cap in the bunghole not in use on each drum lid. Then the purifier was started and the fluid was drawn from the contaminated fluid drum, through the purifier and into the second drum in just under 20 minutes. Following the single pass purification, samples were taken from the top, middle and bottom of the fluid in the second drum and evaluated for particles and water content. The inlet/suction tube from the original contaminated fluid drum was cleaned and then attached to the large bunghole in the lid of the second drum. Cycling of the fluid between the second drum and the purifier was begun with samples taken from the top, middle and bottom of the fluid every 15 minutes for the first hour and then every hour after that until the minimum requirements for cleanliness were reached (NAS 1638 Class 5 for particulates and/or <1.0 mg/mL and <100 ppm water).

#### **Single-Drum Purification Process Configuration**

After the two-drum purification process was completed, six gallons of additional new, clean MIL-PRF-83282 hydraulic fluid was added to the second drum. This was done to make up for the fluid that was not transferred from the original contaminated drum to the second drum and also to make up for fluid lost due to sampling. The inlet/suction and outlet/discharge tubes that were used in the two-drum method were left in place for the single-drum method. A sample from the middle of the fluid was taken and evaluated for particles and water content to confirm the cleanliness of the fluid. The fluid in the drum was then contaminated as previous and cycling of the fluid between the drum and purifier was started immediately (i.e., no waiting/settling period). During the run, samples were taken from the top, middle and bottom of the fluid every 15 minutes for the first hour and then every hour after that until the minimum cleanliness limits were reached (NAS 1638 Class 5 for particulates and <100 ppm water).

This procedure for the single-drum method was repeated using the 18" and 24" discharge/outlet tubes. Also, the fluid in the drum was topped off before each run with approximately 1 gallon of new, clean MIL-PRF-83282 hydraulic fluid to make up for the fluid lost due to sampling.

#### **Results and Discussion**

The results from all of the runs are shown in Tables 1-7. At the beginning of each test run, all of the fluids had a NAS 1638 particle count reading of 12 and water content between 600-700 ppm. Generally, the fluid reached the minimum cleanliness limits within a 2-hour time period. Transferring the fluid from one drum, through the purifier and to another drum seemed to have the greatest effect on contaminant removal. Specifics of each of the test runs are discussed below.

#### **Two-Drum Purification Process Configuration**

#### **Run #1**

The results from the first run using the two-drum purification process configuration are shown in Tables 1 and 2. Prior to adding any contaminants to the new, clean fluid, samples were taken from the top, middle and bottom of the fluid and evaluated for particle count, particle weight and water content. The samples registered a NAS 1638

Class 6 reading for particle count, 0.37 mg/mL for particle weight (top and middle samples) and a range of 91-99 ppm water, all typical for drums of new MIL-PRF-83282 hydraulic fluid.

Since high water content can interfere with the automatic particle count determinations, the Arizona road dust slurry was added first until a sample taken from the middle of the fluid produced a reading of NAS 1638 Class 12. Then distilled water was added incrementally until the water content for the middle fluid sample was at least 600 ppm. A reading of 613 ppm of water was achieved following the addition of 105 mL of distilled water. Then three more samples were taken from the top, middle and bottom of the fluid and analyzed for water with the top and bottom samples also being analyzed for weight of particulate contamination. These samples were designated as initial samples (time = 0). While the particulate weight of the top and bottom samples measured 1.70 and 1.59 mg/mL, respectively, the water readings dropped by up to 10% from the previous reading ranging from 543-596 ppm (569 ppm avg.). This may have been caused by the tendency of water to adhere to the sides of the barrel under saturated conditions. The fluid was then allowed to set for three days with samples taken after each 24-hour period.

After 24 hours, top, middle and bottom fluid samples were taken and analyzed for particle count and water content. All three samples had particle counts of NAS 1638 Class 12, however, the actual particle counts were generally reduced within each size category, especially the 25µm and larger sized particles. The particle counts of the largest sized group, measuring >100µm, decreased by 90% (Table 2). The water contents ranged from 574-608 ppm (594 ppm avg.).

Top, middle and bottom samples were again taken from the fluid after 48 hours and analyzed for particle count and water content. At this point, the particles from the top section of the fluid had settled out enough so that a NAS 1638 Class 11 reading was obtained. The middle and bottom sections remained at NAS 1638 Class 12 though the actual particle counts within each of the particle sized groups continued to decrease. Water content was maintained with readings for the three sections ranging from 576-597 ppm (588 ppm avg.).

After 72 hours, both the top and middle fluid sections of the fluid registered NAS 1638 Class 11 for particle count while the bottom fluid sample remained at NAS 1638 Class 12. Actual particle counts continued to decrease but only significantly for those in the 15-25µm and 25-50µm-sized ranges. Particle weights were measured for the top and bottom samples resulting in 0.864 and 0.836 mg/mL, respectively, a 50% drop from the 0 hour measurement and below the gravimetric cleanliness requirement in the MIL-PRF-83282 specification. Water content again held steady ranging from 589-597 ppm (593 ppm avg.).

After the transfer of the fluid from the original contaminated drum, through the purifier and into the second clean drum, both the water and particulates had been reduced by approximately 50%. Particle counts for the top, middle and bottom samples measured NAS 1638 Class 6, 5 and 6, respectively; while the water content ranged from 288-294 ppm (291 ppm avg.).

Particle count NAS 1638 Class readings for each of the three fluid sections remained in the 5-6 range for the next 45 minutes of cycling the fluid between the second drum and

the purifier. After 1 hour of purification, all three fluid sections were NAS 1638 Class 5 which met the MIL-PRF-83282 cleanliness requirement. The water content continued to decrease during this time but required between 1-2 hours to reach the minimum requirement of <100 ppm.

Particle count NAS 1638 Class, contaminant weight, and water content of the residual fluid in the original contaminated fluid drum measured 12, 1.38 mg/mL and 520 ppm, respectively. The actual particle count readings for the larger particle size groups (>25 $\mu$ m) were high relative to the original starting amounts indicating that settling did occur with the larger particles concentrated at the very bottom of the fluid.

#### Run #2

The second run using the two-drum purification process configuration was carried out similarly to the first run with the results shown in Tables 3 and 4. The particulate slurry and distilled water were added to the clean fluid to give readings for the middle section sample of NAS 1638 Class 12 and 628 ppm for particle count and water content, respectively. The actual quantity of particles measured within each of the particle-sized groups for this run, however, was significantly greater than the first run.

The particle count NAS 1638 Class and water content results for the samples taken from the top, middle and bottom sections to represent time = 0 were 12 and ranged from 625-630 ppm, respectively. Over the next three days, the particle count NAS 1638 Class remained 12 but the water content dropped approximately 10% to a range of 564-585 ppm (576 ppm avg.) for the 72-hour samples. Also, similar to the first run, the actual particle counts within the larger-sized particle groups (>25 $\mu$ m) decreased significantly indicating that settling of these particles was occurring (Table 4). Beginning with the 24-hour samples, the modified sampling technique was introduced. This technique utilized a vacuum connector between the end of the sampling tube and the sample bottle. Applying a slight vacuum to the connector allowed the fluid to be drawn up the tube, through the connector and into the sample bottle (Figure 3).

Following the transfer of the fluid from the original contaminated drum, through the purifier and into the second clean drum, both the water and particulates had been reduced by approximately 50%. Particle count NAS 1638 Classes for the top, middle and bottom samples measured 6, 7 and 6, respectively; while the water content ranged from 300-308 ppm (304 ppm avg.).

During the course of cycling the fluid between the second drum and purifier, the water content dropped in a similar fashion as the first run requiring 2 hours for the top, middle and bottom samples to reach the minimum requirement of <100 ppm. Particle count NAS 1638 Class readings for the top, middle and bottom samples over this time remained at 6 and 7. After 3 hours of cycling, the particle count NAS 1638 Class readings were 5, 4 and 6 for the top, middle and bottom samples, respectively. The original sampling method was used to obtain all three section fluid samples after 4 hours of cycling where the NAS 1638 particle count Classes for the samples met the cleanliness requirement with the results being 5, 4 and 5, respectively. Charts showing the particulate and water removal results for each of the two-drum process configuration runs are shown in figures 6 and 7, respectively.

#### **Single-Drum Purification Process Configuration**

#### 12" Discharge Tube

Results using the single-drum purification process configuration and the 12" discharge tube are shown in Table 5. The fluid was contaminated as previous using the particulate slurry and distilled water to give contamination levels of NAS 1638 Class 12 particulate and 665 ppm water. After 2 hours of cycling the fluid through the purifier, the particulate content had been reduced to the minimum cleanliness requirement of NAS 1638 Class 5. After 3 hours, the water content had been reduced to the minimum cleanliness requirement of <100 ppm with the range of values for the three fluid section samples (top, middle and bottom) being 64-78 ppm (73 ppm avg.).

#### 18" Discharge Tube

Results using the single-drum purification process configuration and the 18" discharge tube are shown in Table 6. The beginning fluid contamination levels were NAS 1638 Class 12 particulate and 700 ppm water. Two hours of cycling the fluid through the purifier were required to reduce the particulate contamination to the minimum cleanliness requirement of NAS 1638 Class 5 (the middle and bottom samples each measured Class 4). Also after this same time period (2 hours), the water content had been reduced to just under the minimum cleanliness requirement of <100 ppm with the range of values for the three fluid section samples being 94-97 ppm (96 ppm avg.).

#### 24" Discharge Tube

Results using the single-drum purification process configuration and the 24" discharge tube are shown in Table 7. The beginning fluid contamination levels were NAS 1638 Class 12 particulate and 672 ppm water. Similar to the 18" discharge tube test, 2 hours of cycling the fluid through the purifier reduced the particulate contamination to the minimum cleanliness limit of NAS 1638 Class 5 (the top and middle samples each measured Class 4). The water content was reduced to under the minimum cleanliness requirement of <100 ppm after 2 hours as well with the range of values for the three fluid section samples being 78-89 ppm (84 ppm avg.).

#### Discharge Tube Comparison

Plots showing a comparison of the particulate and water removal using each of the three discharge tubes are shown in figures 8 and 9, respectively. All three runs reached the minimum level of cleanliness limits (NAS 1638 Class 5 for particulates and <100 ppm water) in 2-3 hours. It may be said that the longer the tube, the better the system operates to remove particulates, but this is not significant or clear-cut based on the results. The plot showing water removal does display a minor advantage to using the longer discharge tube; however, the advantage does not appear to be significant.

#### **Conclusions**

This project evaluated the effectiveness of various hydraulic fluid purification process configurations on the removal of water and particulate contaminants from MIL-PRF-83282 hydraulic fluid in 55 gallon drums. The two primary configurations included a two-drum system; which involved a single pass through the purifier from one drum to another followed by cycling the fluid between the purifier and second drum; and a single-drum system which involved cycling the fluid between the purifier and the single drum

only. The former method included a three-day settling period prior to starting the purification process while the latter configuration evaluated the effects of three different discharge tube lengths on the contamination removal process.

After three days of allowing the contaminated hydraulic fluid to set under ambient conditions, it still registered high levels of particulates (NAS 1638 Class 12) and water (593 ppm). But the actual amounts of particulates within each size category did show a significant decrease over this time, especially for the larger-sized particles, indicating that they were settling out of the fluid (Tables 2 and 4). There was no significant change in the water content or its distribution throughout the fluid.

Following the single pass of the fluid from one drum through the purifier then into a second drum, used in the two-drum method, the level of contamination was reduced by about 50%. The cleanliness requirements, in terms of water and particulates, for MIL-PRF-83282 hydraulic fluid were achieved after 2 hours of cycling the fluid between the drum and the purifier for both the two-drum and single-drum configurations. This would indicate that the single-drum method would suffice to clean the fluid and does not require a second drum or a changing out of the purification unit hoses.

With regard to the variable lengths of discharge tubing, it is not clear as to its effect on the contamination removal process based on the tests run here and the associated results. It does appear that the primary advantage to using a longer discharge tube may be to reduce the level of water contamination more quickly.

While the hydraulic fluid cleaning in drums was successful, that was because we were removing volatile or insoluble (particulate) contaminants. Higher boiling, soluble contaminants like JP-8, engine oil, greases, etc are not capable of being removed via purification so if cleaning of used hydraulic fluid in drums is going to be done, the hydraulic fluid in the drums has to be free of those types of contaminants. Very scrupulous segregation of used oils, greases, fuel must be accomplished to safely purify used hydraulic fluid collected in drums.

#### **Acknowledgements**

The authors would like to gratefully acknowledge Captain John M. Yerger and the AMC Battlelab for funding this research and Charles Tobin, Timothy Jenney and Timothy Reid of the University of Dayton Research Institute for their assistance in setting up and running the test rig and performing sample tests.

Figure 1: Pall portable purification unit



Figure 2: Fluid sampling from drum using the vacuum flask method



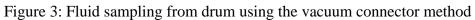




Figure 4: Two-drum (drum-to-drum) purification set-up

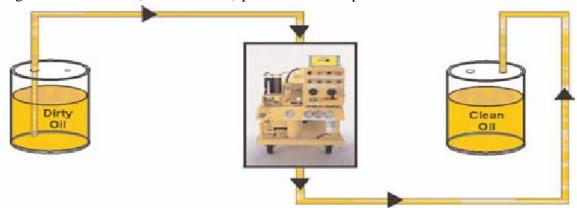


Figure 5: Single-drum purification set-up

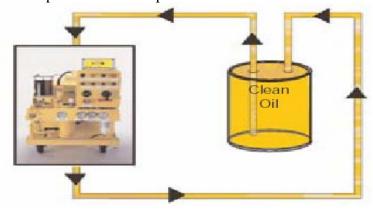


Figure 6: Particulate removal results of the two-drum purification process configuration runs (the drop from NAS 1638 Class 12 to 6 at 0 hours is following the single pass through the purifier)

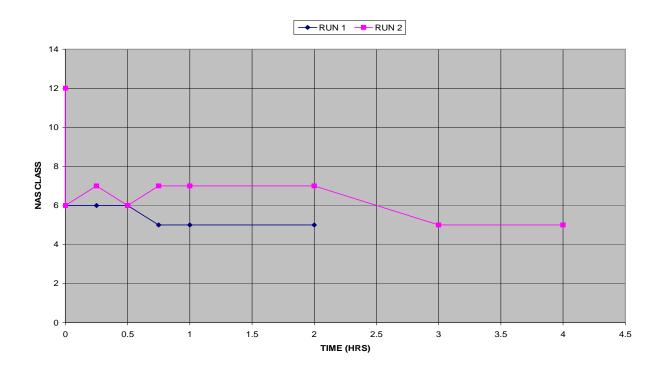


Figure 7: Water removal results of the two-drum purification process configuration runs (the drop in water content at 0 hours is following the single pass through the purifier)

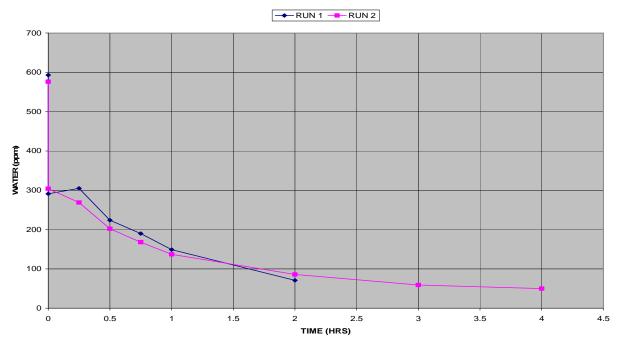


Figure 8: Comparison of particulate removal between three different lengths of discharge tubing using the single-drum purification process configuration

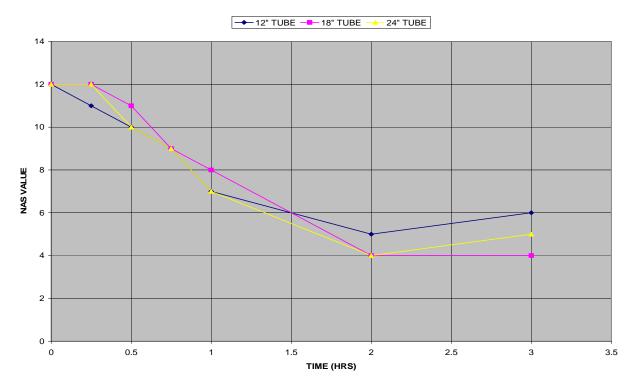


Figure 9: Comparison of water removal between three different lengths of discharge tubing using the single-drum purification process configuration

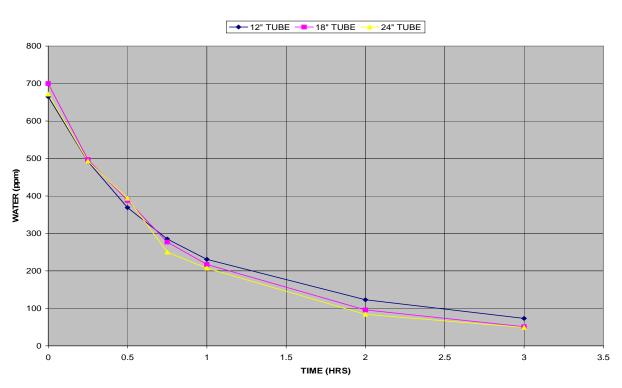


Table 1: Test results from run #1 using the two-drum purification process configuration

			Sampling	PARTICLES		H <sub>2</sub> O PPM
MLO#	Hrs	Comment	Point	NAS 1638	Gravimetric	100 MAX
05-0686	NA	New Fluid	Тор	6	0.37 Top&Mid	99
05-0687	NA	New Fluid	Middle	6	Combined	91
05-0688	NA	New Fluid	Bottom	6	NA	91
No MLO	NA	Contaminated with Particles only	Middle	12	NA	NA
No MLO	NA	Added water after particles	Middle	NA	NA	613
05-0689	0	Contaminated Fld no Purification	Тор		1.70	596
05-0690	0	Contaminated Fld no Purification	Middle	NA	NA	569
05-0691	0	Contaminated Fld no Purification	Bottom		1.59	543
05-0692	24	Contaminated Fld no Purification	Тор	12	NA	574
05-0693	24	Contaminated Fld no Purification	Middle	12	NA	600
05-0694	24	Contaminated Fld no Purification	Bottom	12	NA	608
05-0695	48	Contaminated Fld no Purification	Тор	11	NA	576
05-0696	48	Contaminated Fld no Purification	Middle	12	NA	590
05-0697	48	Contaminated Fld no Purification	Bottom	12	NA	597
05-0698	72	Contaminated Fld no Purification	Тор	11	0.864	592
05-0699	72	Contaminated Fld no Purification	Middle	11	NA	589
05-0700	72	Contaminated Fld no Purification	Bottom	12	0.836	597
05-0701	0	"1" Pass Pall Purifier to New Drum	Тор	6	NA	294
05-0702	0	"1" Pass Pall Purifier to New Drum	Middle	5	NA	290
05-0703	0	"1" Pass Pall Purifier to New Drum	Bottom	6	NA	288
05-0704	0.25	Recycle New Drum with Pall	Тор	6	NA	336
05-0705	0.25	Recycle New Drum with Pall	Middle	5	NA	308
05-0706	0.25	Recycle New Drum with Pall	Bottom	6	NA	270
05-0707	0.5	Recycle New Drum with Pall	Тор	6	NA	219
05-0708	0.5	Recycle New Drum with Pall	Middle	6	NA	239
05-0709	0.5	Recycle New Drum with Pall	Bottom	6	NA	215
05-0710	0.75	Recycle New Drum with Pall	Тор	6	NA	175
05-0711	0.75	Recycle New Drum with Pall	Middle	5	NA	196
05-0712	0.75	Recycle New Drum with Pall	Bottom	5	NA	199
05-0713	1	Recycle New Drum with Pall	Тор	5	NA	140
05-0714	1	Recycle New Drum with Pall	Middle	5	NA	152
05-0715	1	Recycle New Drum with Pall	Bottom	5	NA	156
05-0716	2	Recycle New Drum with Pall	Тор	6	NA	74
05-0717	2	Recycle New Drum with Pall	Middle	6	NA	71
05-0718	2	Recycle New Drum with Pall	Bottom	4	NA	67
05-0723	0	Contam Fld-No Purification-Residual	N/A	12	1.38	520

Table 2: Actual particle amounts over the 3-day settling period from run #1 using the two-drum purification process configuration

			PARTICLE COUNT					
		Sampling	5-15uM	15-25uM	25-50uM	50-100uM	>100uM	NAS 1638
MLO#	Hrs	Point	8000	1408	253	45	8	5
No MLO	0	Middle	532590	62375	15365	1205	45	12
05-0692	24	Тор	519515	44195	4925	140	5	12
05-0693	24	Middle	594980	57070	8425	455	0	12
05-0694	24	Bottom	558470	56895	8620	300	5	12
05-0695	48	Тор	481810	26210	1400	55	0	11
05-0696	48	Middle	551665	32325	2205	60	10	12
05-0697	48	Bottom	549305	36140	2560	40	0	12
05-0698	72	Тор	443760	18155	650	55	0	11
05-0699	72	Middle	486405	23080	1265	55	5	11
05-0700	72	Bottom	512900	27350	1490	95	0	12

Table 3: Test results from run #2 using the two-drum purification process configuration

		ts from run #2 using the two-drui	Sampling	PARTICLES	H <sub>2</sub> O PPM
MLO#	Hrs	Comment	Point	NAS 1638	100 MAX
05-0849	NA	Uncontaminated Fluid	Middle	5	51
No MLO	NA	Contaminated with Particles only	Middle	12	NA
No MLO	NA	Added water after particles	Middle	12	628
05-0861	0	Contaminated Fld no Purification	Тор	12	625
05-0862	0	Contaminated Fld no Purification	Middle	12	628
05-0863	0	Contaminated Fld no Purification	Bottom	12	630
05-0864	24	Contaminated Fld no Purification	Тор	12	534
05-0865	24	Contaminated Fld no Purification	Middle	12	478
05-0866	24	Contaminated Fld no Purification	Bottom	12	467
05-0867	48	Contaminated Fld no Purification	Тор	12	558
05-0868	48	Contaminated Fld no Purification	Middle	12	565
05-0869	48	Contaminated Fld no Purification	Bottom	12	549
05-0870	72	Contaminated Fld no Purification	Тор	12	564
05-0871	72	Contaminated Fld no Purification	Middle	12	585
05-0872	72	Contaminated Fld no Purification	Bottom	12	580
05-0873	0	"1" Pass Pall Purifier to New Drum	Тор	6	300
05-0874	0	"1" Pass Pall Purifier to New Drum	Middle	7	308
05-0875	0	"1" Pass Pall Purifier to New Drum	Bottom	6	303
05-0876	0.25	Recycle New Drum with Pall	Тор	7	251
05-0877	0.25	Recycle New Drum with Pall	Middle	7	278
05-0878	0.25	Recycle New Drum with Pall	Bottom	6	278
05-0879	0.5	Recycle New Drum with Pall	Тор	6	186
05-0880	0.5	Recycle New Drum with Pall	Middle	6	211
05-0881	0.5	Recycle New Drum with Pall	Bottom	6	208
05-0882	0.75	Recycle New Drum with Pall	Тор	7	171
05-0883	0.75	Recycle New Drum with Pall	Middle	7	170
05-0884	0.75	Recycle New Drum with Pall	Bottom	6	164
05-0885	1	Recycle New Drum with Pall	Тор	7	131
05-0886	1	Recycle New Drum with Pall	Middle	6	142
05-0887	1	Recycle New Drum with Pall	Bottom	7	137
05-0888	2	Recycle New Drum with Pall	Тор	7	92
05-0889	2	Recycle New Drum with Pall	Middle	7	96
05-0890	2	Recycle New Drum with Pall	Bottom	6	70
05-0908	3	Recycle New Drum with Pall	Тор	5	71
05-0909	3	Recycle New Drum with Pall	Middle	4	47
05-0910	3	Recycle New Drum with Pall	Bottom	6	60
05-0911	4	Recycle New Drum with Pall	Тор	5	54
05-0912	4	Recycle New Drum with Pall	Middle	4	47
05-0913	4	Recycle New Drum with Pall	Bottom	5	48

Table 4: Actual particle amounts over the 3-day settling period from run #2 using the two-drum purification process configuration

			PARTICLE COUNT					
		Sampling	5-15uM	15-25uM	25-50uM	50-100uM	>100uM	NAS 1638
MLO#	Hrs	Point	8000	1408	253	45	8	5
05-0861	0	Тор	615960	87115	27255	3045	50	12
05-0862	0	Middle	618455	80855	25290	2665	55	12
05-0863	0	Bottom	689215	94500	26100	2430	40	12
05-0864	24	Тор	740175	70440	7925	80	5	12
05-0865	24	Middle	555895	65775	12805	190	5	12
05-0866	24	Bottom	658960	87490	17280	490	0	12
05-0867	48	Тор	681960	21280	875	70	5	12
05-0868	48	Middle	731315	58530	3265	125	10	12
05-0869	48	Bottom	612025	33770	1505	35	0	12
05-0870	72	Тор	655590	9895	580	55	5	12
05-0871	72	Middle	711335	39600	1805	60	5	12
05-0872	72	Bottom	739190	46645	2265	75	0	12

Table 5: Test results from the single-drum purification process configuration using the 12"-long discharge tube

		Sampling	PARTICLES	H <sub>2</sub> O ppm
MLO#	Hrs	Point	NAS 1638	100 MAX
05-0784	0	Middle	12	665
05-0785	0.25	Тор	11	506
05-0786	0.25	Middle	11	484
05-0787	0.25	Bottom	11	487
05-0788	0.5	Тор	10	368
05-0789	0.5	Middle	10	367
05-0790	0.5	Bottom	10	373
05-0791	0.75	Тор	8	283
05-0792	0.75	Middle	9	284
05-0793	0.75	Bottom	9	289
05-0794	1	Тор	7	227
05-0795	1	Middle	7	233
05-0796	1	Bottom	8	233
05-0797	2	Тор	5	124
05-0798	2	Middle	5	112
05-0799	2	Bottom	5	134
05-0839	3	Тор	6*	64
05-0840	3	Middle	7*	77
05-0841	3	Bottom	6*	78
			* Ran Water To	est First

Table 6: Test results from the single-drum purification process configuration using the 18"-long discharge tube

		Sampling	PARTICLES	H <sub>2</sub> O ppm
MLO#	Hrs	Point	NAS 1638	100 MAX
05-0800	0	Middle	12	700
05-0801	0.25	Тор	12	515
05-0802	0.25	Middle	12	500
05-0803	0.25	Bottom	12	476
05-0804	0.5	Тор	10	376
05-0805	0.5	Middle	11	397
05-0806	0.5	Bottom	11	391
05-0807	0.75	Тор	9	277
05-0808	0.75	Middle	9	275
05-0809	0.75	Bottom	9	280
05-0810	1	Тор	7	200
05-0811	1	Middle	8	222
05-0812	1	Bottom	8	229
05-0813	2	Тор	5	97
05-0814	2	Middle	4	94
05-0815	2	Bottom	4	96
05-0845	3	Тор	4	53
05-0846	3	Middle	4	52
05-0847	3	Bottom	4	49

Table 7: Test results from the single-drum purification process configuration using the 24"-long discharge tube

		Sampling	PARTICLES	H₂O ppm
MLO#	Hrs	Point	NAS 1638	100 MAX
05-0816	0	Middle	12	672
05-0817	0.25	Тор	11	446
05-0818	0.25	Middle	12	500
05-0819	0.25	Bottom	12	533
05-0820	0.5	Тор	10	378
05-0821	0.5	Middle	10	398
05-0822	0.5	Bottom	11	407
05-0823	0.75	Тор	8	218
05-0824	0.75	Middle	9	268
05-0825	0.75	Bottom	9	264
05-0826	1	Тор	5	184
05-0827	1	Middle	7	220
05-0828	1	Bottom	8	218
05-0829	2	Тор	4	78
05-0830	2	Middle	4	84
05-0831	2	Bottom	5	89
05-0848	3	Тор	5	50
05-0849	3	Middle	5	51
05-0850	3	Bottom	4	46